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# LISTING OF THE CLAIMS

This listing of the claims will replace all prior versions and listings of claims in the application.

## 1 - 14. (Canceled)

- 15. (Currently Amended) An integrated process for dewaxing a raffinate feedstock containing at least 7270 wppm and up to 20,000 ppmw sulfur and up to 1000 ppmw nitrogen which consists essentially of: (a) contacting the feedstock without prior hydrotreatment with a dewaxing catalyst consisting essentially of ZSM-48 under hydrodewaxing conditions, said dewaxing catalyst including a metal hydrogenation component which is at least one Group 6 metal, at least one Group 8-10 metal, or mixtures of Group 6 and Group 8-10 metals, to form a hydrodewaxed product, and (b) passing at least a portion of the hydrodewaxed product and gaseous components from step (b) without disengagement to a hydrofinishing zone containing a MCM-41 catalyst and hydrofinishing the hydrodewaxed product under hydrofinishing conditions.
- 16. (Original) The process of claim 15 wherein the metal hydrogenation component is Pt, Pd or mixtures thereof.
- 17. (Original) The process of claim 15 wherein the hydrodewaxing conditions include a temperature of 360 to 425°C, hydrogen pressures of from 2859-20786 kPa, liquid hourly space velocities of 0.1 to 10 LHSV and hydrogen treat gas rates of from 53.4-1780 m<sup>3</sup>/m<sup>3</sup>.
- 18. (Original) The process of claim 15 wherein the hydrofinishing conditions include temperatures of 150-350°C, pressures of 100-3000 psig (790-20786 kPa), LHSV of 0.1-20, and treat gas rates of 300-10000 scf/bbl (53-1780 m<sup>3</sup>/m<sup>3</sup>).

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### 19. (Canceled)

- 20. (Currently Amended) An integrated process for dewaxing a raffinate feed which consists essentially of:
  - (a) solvent dewaxing the raffinate to form a raffinate and a slack wax,
  - (b) deoiling the slack wax to produce a foots oil,
  - (c) in a first-reactor contacting the foots oil with a hydrotreating catalyst under hydrotreating conditions to produce a hydrotreated foots oil and gaseous nitrogen- and sulfur-containing contaminants,
  - (d) passing at least a portion of the hydrotreated foots oil and gaseous sulfur- and nitrogen-containing contaminants from step (c) without disengagement to a second reactor containing a hydrodewaxing zone that consists essentially of a ZSM-48 dewaxing catalyst and hydrodewaxing the hydrotreated foots oil under hydrodewaxing conditions, said dewaxing catalyst including a metal hydrogenation component which is at least one Group 6 metal, at least one Group 8-10 metal, or mixtures of Group 6 and Group 8-10 metals to form from a hydrodewaxed product, and
  - (e) passing at least a portion of the hydrodewaxed product from step (d) without disengagement to a hydrofinishing zone containing a MCM 41 hydrofinishing catalyst and hydrofinishing under hydrofinishing conditions.

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- 21. (Original) The process of claim 20 wherein the hydrotreating conditions temperatures of 315-425°C., pressures of 2170-20786 kPa, Liquid Hourly Space Velocities (LHSV) of 0.1-10 and hydrogen treat rates of 89-1780 m<sup>3</sup>/m<sup>3</sup>.
- 22. (Original) The process of claim 20 wherein the metal hydrogenation component is Pt, Pd or mixtures thereof.
- 23. (Original) The process of claim 20 wherein the hydrodewaxing conditions include a temperature of 360 to 425°C., hydrogen pressures of from 2859-20786 kPa, liquid hourly space velocities of 0.1 to 10 LHSV and hydrogen treat gas rates of from 53,4-1780 m<sup>3</sup>/m<sup>3</sup>.

## 24. (Canceled)

- 25. (Currently Amended) The process of claim 20 wherein the slack wax or foots oil is blended with raffinate feed prior to step  $G(\underline{c})$ . 26 37. (Canceled)
- 38. (New) The process of claim 15, wherein the hydrofinishing zone contains a MCM-41 hydrofinishing catalyst.
- 39. (New) The process of claim 20, wherein the hydrofinishing zone contains a MCM41 hydrofinishing catalyst.